

## GAS-OIL RATIO CORRELATION ( $R_s$ ) FOR GAS CONDENSATE USING GENETIC PROGRAMMING

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КОРРЕЛЯЦИЯ ГАЗСОДЕРЖАНИЯ ( $R_s$ ) ДЛЯ ГАЗОВОГО КОНДЕНСАТА, С ИСПОЛЬЗОВАНИЕМ ГЕНЕТИЧЕСКОГО ПРОГРАММИРОВАНИЯ

**K. A. Fattah**  
Petroleum and Natural Gas Engineering  
Department, College of Engineering,  
King Saud university, P.O. 800, Riyadh  
11421, Saudi Arabia.  
On leave from Faculty of engineering,  
Cairo university

**К. А. Фаттах**  
Факультет технологии нефти и  
природного газа, Инженерный  
колледж при университете короля  
Сауда, Р.О. 800, Riyadh 11421,  
Саудовская Аравия

A new correlation for solution gas oil ratio (RS) for gas condensate reservoir was developed in this paper by using genetic programming algorithm of a commercial software (Discipulus) program. Matching PVT experimental data with an equation of state (EOS) model in a commercial simulator (Eclipse simulator) was used to calculate the solution gas oil ratio (RS) values used in this study. More than 1800 solution gas oil ratio (RS) values obtained from the analysis of eight gas condensate fluid PVT laboratory reports, selected under a wide range of reservoir temperature and pressure, composition and condensate yield, were used.

Comparisons of the results showed that currently published correlations of gas oil ratio (RS) for gas condensate gave poor estimates of its value, (the average absolute error for sanding correlation was 63.48 with a standard deviation equal to 0.724, the average absolute error for Glaso correlation was 61.19 % with a standard deviation equal to 0.688, the average absolute error for Vasques and Beggs correlation was 52.22 % with a standard deviation equal to 0.512, the average absolute error for Marhoun correlation was 56.34 % with a standard deviation equal to 0.519 and the average absolute error for Fattah et al correlation was 18.6 % with a standard deviation equal to 0.049).

The proposed new correlation improved extensively the average absolute error for gas condensate fluids. The average absolute error for the new correlation was 10.54 % with a standard deviation equal to 0.035. Also, the hit-rate (R2) of the new correlation was 0.9799 and the fitness variance was 0.012.

The important of the new correlation comes from being depends only on readily available production data in the field and can have wide applications when representative PVT lab reports are not available.

В данной работе представлена разработка новой корреляции газосодержания (RS) для газоконденсатной залежи с использованием алгоритма генетического программирования коммерческого программного обеспечения (Discipulus). Для вычисления значений газосодержания (RS), используемых в данном исследовании, было применено сопоставление экспериментальных PVT-данных с моделью уравнения состояния (EOS) в коммерческом имитаторе (имитатор Eclipse). Было использовано более 1800 значений газосодержания (RS), полученных из лабораторных отчетов о PVT-анализе восьми газоконденсатных флюидов, отобранных при широком диапазоне показателей температуры и давления, состава и выхода конденсата.

Сравнения результатов показали, что имеющиеся опубликованные корреляции газосодержания (RS) для газоконденсата давали некачественные определения его значения (средняя абсолютная ошибка для корреляции Standing составляла 63.48 при среднеквадратичном отклонении равном 0.724, средняя абсолютная ошибка для корреляции Glaso была 61.19% при среднеквадратичном отклонении равном 0.688, средняя абсолютная ошибка для корреляции Vasques и Beggs составляла 52.22 % при среднеквадратичном отклонении 0.512, средняя абсолютная ошибка для корреляции Marhoun составляла 56.34% при среднеквадратичном отклонении равном 0.519, и средняя абсолютная ошибка для корреляции Fattah и др. составляла 18.6% при среднеквадратичном отклонении 0.049.)

Предложенная новая корреляция значительно улучшила показатель средней абсолютной ошибки для газоконденсатных флюидов. Средняя абсолютная ошибка для новой корреляции составила 10.54% при среднеквадратичном отклонении равном 0.035. А также коэффициент детерминации (R2) новой корреляции составил 0.9799, а вероятность ошибки - 0.012.

Актуальность новой корреляции вытекает из того, что она зависит только от легкодоступных промысловых данных на месторождении, и может широко применяться при отсутствии типичных лабораторных отчетов по PVT-испытаниям.

**Key words:** Gas-oil ratio Correlation; PVT laboratory report; Genetic programming; Gas condensate; modified black oil simulation.

**Ключевые слова:** корреляция газосодержания; лабораторный отчет о PVT-анализе; генетическое программирование; газовый конденсат; модифицированная модель «блэк ойл».

### Introduction

Material balance equation is a useful method of reservoir performance analysis. It is routinely used to

estimate oil, and gas reserves and predict future reservoir performance. Schilthuis, in 1936, was among the first to formulate and apply material balance analysis. As time progressed, more sophisticated material balance models evolved, each striving for greater generality.

Application of two-hydrocarbon-component, zero-dimensional material balance model had been restricted to black-oil or dry-gas reservoirs. As gas condensate reservoirs exploration increases, there has been a growing need to address this limitation.

Spivak and Dixon (1973) introduced the Modified Black Oil (MBO) simulation approach. The PVT functions for modified black oil (MBO) simulation and material balance calculations of gas condensate are (condensate-gas ratio,  $R_v$ , solution gas-oil ratio,  $R_s$ , oil formation volume factor,  $B_o$ , and gas formation volume factor,  $B_g$ ). The MBO approach assumes that stock-tank liquid component can exist in both liquid and gas phases under reservoir conditions in gas condensate reservoir.

A few authors have addressed the question of how to best generate the PVT properties for gas condensate. Whitson and Torp (1983) used laboratory constant volume depletion (CVD) data to calculate “modified black oil” PVT fluid properties  $B_o$ ,  $R_s$ ,  $B_g$  and  $R_v$  for gas condensate fluids. Coats (1985) suggested a different approach from Whitson and Torp’s (W&T) to calculate the modified black oil properties for gas condensates. Walsh and Towler (1994) suggested a new simple method to compute the black-oil PVT properties of gas condensate reservoirs. Fevanget *et al.* (2000) presented guidelines to help engineers choose between MBO and compositional approaches. Fattah *et al.* (2009) presented new correlations to develop MBO PVT properties when PVT fluid samples reports are not available.

Most of the methods in the literature for generating modified black oil PVT fluid properties ( $B_o$ ,  $R_s$ ,  $B_g$  and  $R_v$ ) for gas condensate need a combination of lab experiments and elaborate calculation procedures.

This study involves two parts: the first part includes a comparison between the different correlations used to calculate the solution gas oil ratio ( $R_s$ ) for gas condensate to determine the most accurate one. The second part involves the development of a new correlation to calculate  $R_s$  for gas condensate reservoir using Genetic algorithm methods. Validation of the new correlation is achieved through comparison between the new correlation value of  $R_s$  and  $R_s$  generated by Whitson and Torp method from PVT lab data.

### Fluid Samples

Eight gas condensates (GC) samples are used in this study. The samples were obtained from reservoirs representing different locations and depth, and were selected to cover a wide range of gas condensate fluid characteristics. Some samples represent near critical fluids as explained by McCain and Bridges (1994). Table 1 presents a description of the major properties of these eight fluid samples.

EOS models in a commercial simulator (Eclipse simulator) were used to develop an EOS model for each sample in Table 1. Tuning the EOS model that matched as best as possible the experimental results of all available PVT laboratory experiments (CCE, DL, CVD, and separator tests) was constructed. The procedure suggested by Coats and Smart (1986) to match the laboratory results was followed. For consistency, all EOS models were developed using Peng and Robinson

(1976) EOS with volume shift correction (3-parameter EOS).

### Approach

The developed EOS model for each sample in table 1 was used to output MBO PVT properties ( $R_v$ ,  $R_s$ ,  $B_o$ , and  $B_g$ ) at six different separator conditions using Whitson and Torp (1983) procedure. The extracting data for the MBO PVT properties involves 1836 points from the different eight gas condensate samples. The first part was to compare between the extracted  $R_s$  and the most common  $R_s$  correlations to determine the most accurate one.

The second part involved the development of a new correlation to calculate  $R_s$  for gas condensate reservoir using Genetic algorithm program.

### Genetic Programming

Genetic algorithms, evolution strategies and genetic programming belong to the class of probabilistic search procedures known as Evolutionary Algorithms that use computational models of natural evolutionary processes to develop computer-based problem solving systems. Solutions are obtained using operations that simulate the evolution of individual structures through mechanism of reproductive variation and fitness based selection. Due to their reported robustness in practical applications, these techniques are gaining popularity and have been used in a wide range of problem domain. The main difference between genetic programming and genetic algorithm is the representation of the solution. Genetic programming creates computer programs as solution whereas genetic algorithm creates a string of numbers to represent the solution. Genetic programming is based on the Darwinian principle of reproduction and survival of the fittest and analogs of naturally occurring genetic operations such as crossover and mutation (Koza, 1992). Genetic programming uses four steps to solve a problem (Koza, 1997):

- 1) Generate an initial population of random compositions of the functions and terminals (input) of the problem
- 2) Execute each program in the population and assign a fitness value.
- 3) Create a new offspring population of computer programs by copying the best programs and creating new ones by mutation and crossover.
- 4) Designation of the best computer program in the generation.

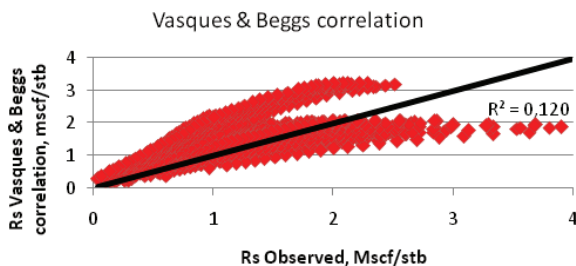
### Solution Gas Oil Ratio ( $R_s$ ) correlations

This part presented the comparison between the common correlations used to calculate the solution gas oil ratio ( $R_s$ ) for gas condensate in the literature. The comparison of the Vasques and Beggs correlation (1980) with the observed  $R_s$  for gas condensate result in average absolute error was 52.22 % with a standard deviation

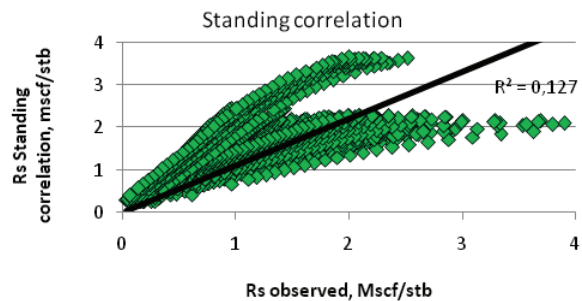
**Table 1.** Characteristics of Fluid Samples

Property	GC 1	GC 2	GC 3	GC 4	GC 5	GC 6	GC 7	GC 8
Reservoir Temperature (°F)	312	286	238	256	186	312	300	233
Initial Reservoir Pressure (psig)	14216	NA	6000	7000	5728	14216	5985	17335
Initial Producing Gas-Oil ratio(SCF/STB)	3413	4278	NA	4697	5987	8280	6500	6665
Stock Oil gravity (° API)	45.6	NA	NA	46.5	58.5	50.7	45.6	43
Saturation Pressure (psig)	5210	5410	4815	6010	4000	5465	5800	11475
Components	Composition (Mole %)							
CO <sub>2</sub>	2.66	4.48	0.14	0.01	0.18	2.79	6.98	0.36
N <sub>2</sub>	0.17	0.70	1.62	0.11	0.13	0.14	1.07	0.31
C <sub>1</sub>	59.96	66.24	63.06	68.93	61.72	66.73	65.25	81.23
C <sub>2</sub>	7.72	7.21	11.35	8.63	14.1	10.22	8.92	5.54
C <sub>3</sub>	6.50	4.00	6.01	5.34	8.37	5.90	4.81	2.66
iC <sub>4</sub>	1.93	0.84	1.37	1.15	0.98	1.88	0.85	0.62
nC <sub>4</sub>	3.00	1.76	1.94	2.33	3.45	2.10	1.75	1.06
iC <sub>5</sub>	1.64	0.74	0.84	0.93	0.91	1.37	0.65	0.47
nC <sub>5</sub>	1.35	0.87	0.97	0.85	1.52	0.83	0.69	0.52
C <sub>6</sub>	2.38	0.96	1.02	1.73	1.79	1.56	0.83	0.84
C <sub>7+</sub>	<b>12.69</b>	<b>12.2</b>	<b>11.68</b>	<b>9.99</b>	6.85	6.48	8.2	6.39

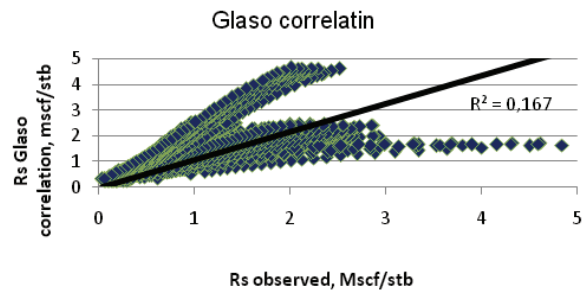
equal to 0.512. Figure1 presents cross-plots for  $R_s$  (Vasques & Beggs) vs.  $R_s$  (Observed) for gas Condensate samples. The comparison of the Standing correlation (1947) results in average absolute error was 63.48 % with a standard deviation equal to 0.724. Fig. 2 shows cross-plots for Standing correlation. The comparison of the Glaso correlation (1980) results in average absolute error was 61.19 % with a standard deviation equal to 0.688. Fig. 3 displays cross-plots for Glaso correlation. The comparison of the Marhoun correlation (1988) results in average absolute error was 56.34 % with a standard deviation equal to 0.519. Figure4 presents cross-plots for Glaso correlation. The comparison of the Fattah et al correlation (2009) results in average absolute error was 18.66 % with a standard deviation equal to 0.049, which is the best correlation in the literature. Figure5 shows cross-plots for Fattah et al correlation.



**Figure 1.**  $R_s$  for gas Condensate samples cross-plot for Vasques&Beggs correlation



**Figure 2.**  $R_s$  for gas Condensate samples cross-plot for Standing correlation



**Figure 3.**  $R_s$  for gas Condensate samples cross-plot for Glaso correlation

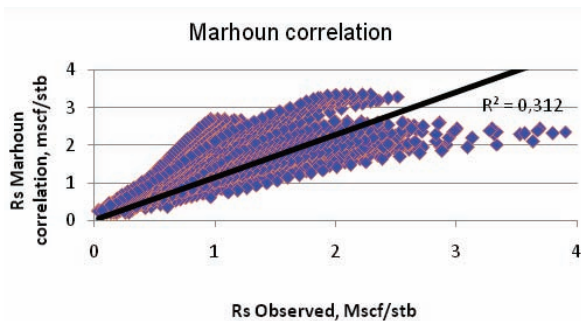


Figure 4.  $R_s$  for gas Condensate samples cross-plot for Marhoun correlation

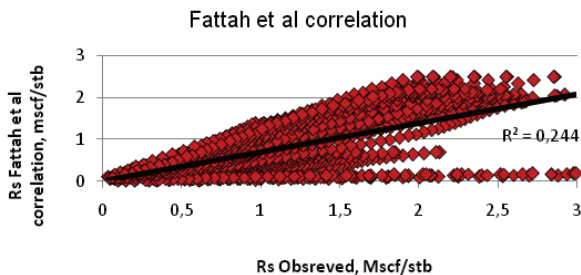


Figure 5.  $R_s$  for gas Condensate samples cross-plot for Fattah et al correlation

### Developed Gas-oil ratio correlation ( $R_s$ ) for gas condensate Using Genetic Program

The second part in this study involved the development of the new correlation to calculate  $R_s$  for gas condensate reservoir using genetic algorithm program. A commercial Genetic Programming system called *Discipulus* was used to develop the new  $R_s$  correlation (J. A. Foster, 2001, F. D. Francone, 2004). “Discipulus is a steady state genetic programming system, using tournament selection in which two pairs of individuals compete each round for reproduction. All the usual parameters can be adjusted with Discipulus: crossover rate, mutation rate, population size, instruction set, distribution of initial program sizes, termination criteria, and parsimony pressure (fitness advantages for smaller programs).”, (J. A. Foster, 2001). The input data files for this software are classified into three semi-equal groups, “training data”, «validation data» and «applied data». These input files include measured inputs and outputs parameters for our correlation.

The inputs parameters for our correlation are:

- Pressure (P), psi,
- Reservoir temperature (T),  $R^\circ$ ,
- API gravity of the reservoir fluid,
- Specific gravity of surface gas ( $SG_g$ )
- Specific gravity of surface oil ( $SG_o$ )

The output is the solution gas oil ratio,  $R_s$ .

Discipulus program gives different types of data and charts that show how the run in progress improved its performance. Discipulus creates thousands models (programs) from given data files that allow us to predict outputs from similar inputs and for each model

(program) gives us his performance, (the hit-rate ( $R^2$ ) and the fitness variance). At the end of the run, we choose the best model (program) depending on its hit-rate ( $R^2$ ) and fitness variance to calculate the solution gas oil ratio;  $R_s$ . The models are creates as computer programs in Java, C++ code, or assembler program.

Figure6 shows the fitness improvement of the best genetic program for our correlation with time. The hit-rate ( $R^2$ ) of the best genetic program, (the new correlation), was 0.9799 and the fitness variance was 0.012. Figs 7-9 present the match between the observed  $R_s$  and the calculated  $R_s$  for the new correlation. Each figure show that the match between all input points of the observed  $R_s$  and the calculated  $R_s$  for the same point from the best program developed by the software, the best team (During a project, Discipulus assembles the best programs into teams. The output from all of the programs that comprise a team are assembled into one collective output that is frequently better than any particular member of the team), and the selected program (almost is the best program if the default of the software is not changed). The results for our case indicated that the new correlation (best program) almost completely matches the observed  $R_s$  data. For more model validation, cross plots between observed and calculated  $R_s$  was drawn (Figure10) and the average absolute error and the standard deviation for the new correlation was calculated and equal to 10.54 % and 0.035 respectively. Table 2 summarizes the statistical comparison between the different correlations and the new correlation. From this table, we found that the new correlation is the best matched correlation.



Figure 6. The program fitness improvement with time

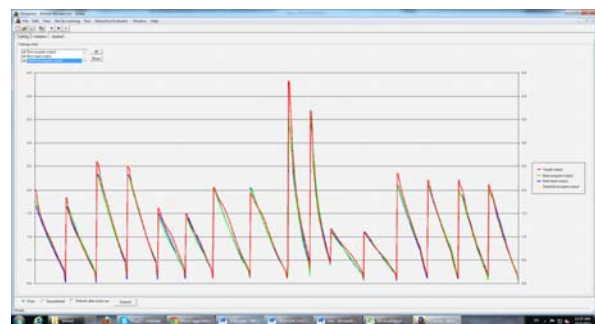


Figure 7. The observed VS calculated  $R_s$  data for training input data

Table 2. Statistical comparison of all correlations using observed data

Vas & Beggs correlation		Standing correlation		Glaso correlation		Marhoun correlation		Khaled correlation		new correlation	
AAE	SD	AAE	SD	AAE	SD	AAE	SD	AAE	SD	AAE	SD
52.2 %	0.51	63.4 %	0.73	61.2 %	0.69	56.3 %	0.52	18.6 %	0.05	10.5 %	0.035

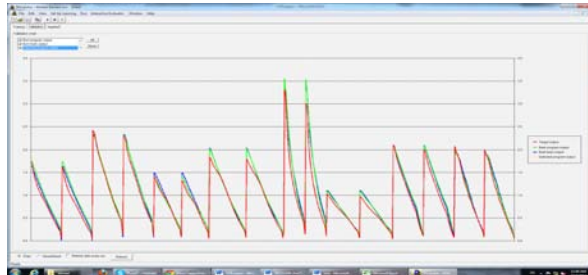


Figure 8. The observed VS calculated  $R_s$  dataform validation input data

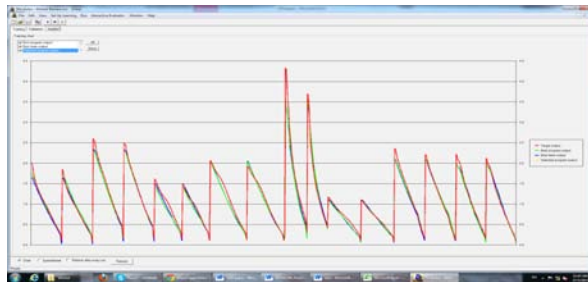


Figure 9. The observed VS calculated  $R_s$  dataform applied input data

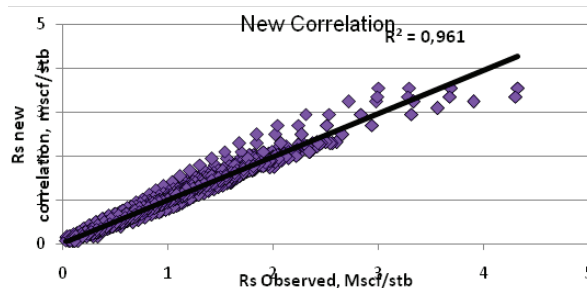


Figure 10.  $R_s$  for gas Condensate samples cross-plot for New correlation

The output C++ code of the genetic Model from the Discipulus to calculate the new  $R_s$  correlation was given in the appendix. This code was used with C++ compiler to develop a windows interface program to calculate  $R_s$  (Figure 11). This code can be modified to generate a solution gas oil ratio array for different temperature, pressure values of a given reservoir.

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A COMPUTER PROGRAM TO CALCULATE THE GAS OIL RATIO FOR GAS
CONDENSITE USING GENETIC PROGRAMING

<<<INPUT DATA>>
Inter PRESSURE value <psia> = 1000
Inter TEMPERATURE value <R> = 689
Inter API value = 47.3255
Inter OIL S.C value = 0.79127
Inter GAS S.C value = 0.91896

<<<OUTPUT DATA>>
The GAS OIL RATIO ARE <Mscf/STB> = 0.159353
    
```

Figure 11. The windows interface of the program

The new correlation presented in this work can be used with other set of correlations to generate MBO PVT properties for material balance calculation, or reservoir simulation without the need for fluid samples or elaborate procedure for EOS calculations. The application of these correlations is of particular importance especially when representative fluid samples are not available.

### Conclusions

Based on work presented in this study, the following conclusions were made:

1. The comparison of the literature gas oil ratio correlations for gas condensate result in Fattah et al correlation was the best correlation to calculate gas oil ratio RS with average absolute error was 18.66 % and a standard deviation equal to 0.049.
2. New RS correlation was developed for gas oil ratio RS of gas condensates. The Discipulus software, a commercial Genetic Programming system, was used to develop the new correlation program. It is based on the concept of genetic algorithm.
3. The hit-rate ( $R^2$ ) of the new correlation was 0.9799 and the fitness variance for the new correlation was 0.012.
4. The comparison of the new correlation with the observed gas oil ratio RS result in average absolute error was 10.54 % with a standard deviation equal to 0.035.

### Выводы

На основании работы, представленной в данном исследовании, были сделаны следующие выводы:

1. Результаты сравнения опубликованных корреляций для газоконденсата показали, что лучшей корреляцией для вычисления газосодержания RS стала корреляция Фаттаха и др. (Fattah et al), в которой

средняя абсолютная ошибка составила 18,6% при среднеквадратичном отклонении 0,049.

2. Для газосодержания RS газоконденсатов была разработана новая корреляция RS. Для разработки новой корреляционной программы было использовано программное обеспечение Discipulus, коммерческая система генетического программирования. Оно основывается на концепции генетического алгоритма.

3. Коэффициент детерминации (R<sup>2</sup>) новой корреляции составил 0,9799, а вероятность ошибки – 0,012

4. Сравнение новой корреляции с наблюдаемым газосодержанием RS показало, что средняя абсолютная ошибка для новой корреляции составляет 10,54% при среднеквадратичном отклонении равном 0,035.

## REFERENCES

1. Ahmed, T.: Hydrocarbon Phase Behavior, Gulf Publishing Company, Houston, 1989.

2. Coats, K.H.: "Simulation of Gas Condensate Reservoir Performance," paper SPE 10512, published at the JPT, Oct.1985, pp. 1870-1886.

3. Coats, K.H. and Smart, G.T.: "Application of a Regression-Based EOS PVT Program to Laboratory Data," SPERE (May 1986) 277-299.

4. Cook, R.E., Jacoby, R.H., and Ramesh, A.B.: "A Beta-Type Reservoir Simulation for Approximating Compositional Effects during Gas Injection," paper SPE 4272, SPEJ (Oct. 1974), 471-481.

5. Craft, B.C., Hawkins, M., and Terry, R.E.: Applied Petroleum Reservoir Engineering, Second edition" Prentice-Hall, Inc., New Jersey, 1991.

6. ECLIPSE suite of programs (Schlumberger, 2005).

7. Fattah, K. A: Volatile Oil and Gas Condensate Fluid Behavior for Material Balance Calculations and Reservoir Simulation, Ph.D. Thesis, Cairo University, Egypt 2005.

8. Fattah, K. A., El-Banbi, A. H., and Sayyoub, M.H.: "New correlations calculate volatile oil, gas condensate PVT properties" Oil& Gas Journal, May 25, 2009.

9. Foster, J. A.: "Review: Discipulus: A Commercial Genetic Programming System" Register Machine Learning Technologies, 2001.

10. Francone, F. D.: "Discipulus, Owner's Manual" Machine Learning Technologies, 2004.

11. Glaso, O.: "Generalized Pressure-Volume-Temperature Correlations," JPT, May 1980.

12. Havlena, D., and Odeh, A.H.: "The Material Balance as an Equation of a straight Line," JPT, Aug., 1963. pp. 896-900; Trans. AIME vol. 228.

13. Marhoun, M. A.: "PVT Correlation for Middle East Crude Oils," JPT, May 1988.

14. McCain, W. Jr., "Analysis of Black Oil PVT Reports Revisited," paper SPE 77386, October 2002.

15. McCain, W. Jr., "Reservoir-Fluid Property Correlations-State of the Art," SPERE, May 1991.

16. McCain, W. Jr., and Spivey, J. P.: "Extrapolation of Laboratory Measured Black Oil and Solution Gas Fluid Properties for Variable Bubble point Simulation," SPE paper 56746, October 1999.

17. McCain, W. Jr., The Properties of Petroleum Fluids, Second Edition" PennWell Publishing company, Tulsa, Oklahoma, 1990.

18. McVay, D.A.: Generation of PVT Properties for Modified Black-Oil Simulation of Volatile Oil and Gas Condensate Reservoirs, Ph.D. Thesis, Texas A&M University, TX. 1994.

19. Peng, D.Y. and Robinson, D.B. "A New Two-Constant Equation of State," Ind. and Eng. Chem. Fund. (1976) 15, 59.

20. Schilthuis, R.J.: "Active Oil and Reservoir Energy," Trans. AIME 1936, 148, pp. 33-52.

21. Spivak, V.J. and Dixon, T.N.: "Simulation of Gas Condensate Reservoir," paper SPE 4271 presented at the 3rd Numerical Simulation of Reservoir Performance Symposium, Houston, Jan. 10-12, 1973.

22. Standing, M. B., "A Pressure-Volume-Temperature Correlation for Mixture of California Oils and Gases," Drilling and Production Practice, API, 1957, pp. 275-287.

23. Vasques, M. and Beggs, H. D.: "Correlation for Fluid Physical Property Prediction," JPT, June 1980.

24. Walsh, M.P., Ansah, J., and Raghavan, R.: "The New Generalized Material Balance As an equation of a Straight -Line: Part 1- Application to undersaturated and Volumetric Reservoir," paper SPE 27684 presented at the 1994 society of petroleum engineers Permian Basin Oil and Gas

recovery Conference, March 16-18, Midland TX.

25. Walsh, M.P., Ansah, J., and Raghavan, R.: "The New Generalized Material Balance As an equation of a Straight -Line: Part 2- Application to Saturated and Non-Volumetric Reservoir," paper SPE 27728 presented at the 1994 SPE Permian Basin Oil and Gas recovery Conference, Midland TX, March 16-18.

26. Walsh, M.P., Towler, B.F.: "Method Computes PVT Properties for Gas Condensate," OGI, July 31, 1994, pp. 83-86.

27. Walsh, M.P.: "A Generalized Approach to Reservoir Material Balance calculations," paper presented at the International Technical Conference of Petroleum Society of CIM, Calgary, Canada, May 9-13, 1993, accepted for publication, JCPT, 1994.

28. Walsh, M.P.: "New, Improved Equation Solves for Volatile Oil and Condensate Reservoirs," OGI, Aug. 22, 1994, pp. 72-76.

29. Whitson, C.H., and Trop, S.B.: "Evaluating Constant-Volume Depletion Data," paper SPE 10067, SPE, Richardson, TX. USA, 1983.

*K. A. Fattah, Assistant Professor in Petroleum and Natural Gas Engineering Department, College of Engineering, King Saud university, P.O. 800, Riyadh 11421, Saudi Arabia.*

*On leave from Faculty of engineering, Cairo university.  
E\_mailkelshreef@ksu.edu.sa*

*K. A. Фаттах, Доцент факультета технологии нефти и натурального газа, Инженерный колледж, Университет короля Сауда, P.O. 800, Riyadh 11421, Саудовская Аравия.*

*По поручению инженерного факультета Каирского университета.  
E\_mailkelshreef@ksu.edu.sa*